

Kongeriget Danmark

Patent application No.:

PA 2003 00954

Date of filing:

25 June 2003

Applicant:

(Name and address)

Pharmexa A/S

Kogle Allé 6

DK-2970 Hørsholm

Denmark

Title: Purification of her-2 variants

IPC: -

This is to certify that the attached documents are exact copies of the above mentioned patent application as originally filed.



PRIORITY DOCUMENT

REC'D 2 6 JUL 2004

WIPO

SUBMITTED OR TRANSMITTED IN COMPLIANCE WITH RULE 17.1(a) OR (b)

Patent- og Varemærkestyrelsen Økonomi- og Erhvervsministeriet

20 July 2004

Susanne Morsing

PATENT- OG VAREMÆRKESTYRELSEN

1

Modtaget PVS 25 Jülii 2003

PURIFICATION OF HER-2 VARIANTS

FIELD OF THE INVENTION

The present invention relates to the field of affinity purification of proteins. More particularly, the present invention relates to improvements in metal affinity protein purification, especially purification of histidine tagged or histidine rich proteins that have been recombinantly produced in insect cells. The invention also relates to specific purification schemes suitable for histidine-tagged protein variants derived from the EGFR (endothelial growth factor receptor) family of proteins, especially the cancer-associated antigen HER-2.

Further, the present invention relates to an immunogenic variant of human HER-2 that is capable of raising an immune 15 response in humans, which also targets the native human HER-2 molecule.

BACKGROUND OF THE INVENTION

The cancer associated membrane protein HER-2 is a member of the EGFR family of proteins. This particular protein has shown 20 promise as an immunogen in active specific immunotherapy of certain cancers, notably breast cancer and colorectal cancer.

The assignee of the present patent application has previously filed patent applications relating to active vaccination against the HER-2 antigen, cf. WO 00/20027 which is hereby 25 incorporated by reference herein. Further research in this field has now identified preferred HER-2 variants for such vaccines, but a general problem in protein chemistry is to

15450DX00

2

devise improved means for obtaining satisfactory yields of recombinant protein with a high degree of purity.

Immobilized metal ion affinity chromatography (IMAC) was first introduced by Porath (Porath, J., J. Carlsson, I. Olsson, G. 5 Belfrage [1975] Nature 258:598-599.) under the term metal chelate chromatography and has been previously reviewed in several articles (Porath, J. [1992] Protein Purification and Expression 3:263-281; and articles cited therein). The IMAC purification process is based on the employment of a chelating 10 matrix loaded with soft metal ions such as Cu²⁺ and Ni²⁺. Electron-donating groups on the surface of proteins, especially the imidazole side chain of histidine, can bind to The non-coordinated sites of the loaded metal. The interaction between the electron donor group with the metal can be made 15 reversible by lowering the pH or by displacement with imidazole. Thus, a protein possessing electron-donating groups such as histidine can be purified by reversible metal complex/protein interactions.

In 1991, Ford et al. (Ford, C., I. Suominen, C. Glatz [1991]
20 Protein Expression and Purification 2:95-107) described protein purification using IMAC technology (Ni-NTA ligand) as applied to recombinant proteins having tails with histidine residues (polyhistidine recombinant proteins, "His-tagged proteins"). This method takes advantage of the fact that two or more histidine residues can cooperate to form very strong metal ion complexes.

Numerous variations of this technology exists, where the histidine residues are attached as "tags" to the relevant recombinant protein in various combinations, e.g. including 30 recognition sites for specific proteases so that the his tag can be subsequently removed enzymatically.

15450DX00

3

Expression of proteins in insect cells require the use of various specialised culture media and also entails contamination of the recombinant protein with various insect cell derived constituents that are not found in bacteria, fungi and mammalian cells. Purification schemes devised for recombinant proteins produced in bacteria, fungi, or mammalian cells are therefore not necessarily the optimum choice when a protein produced in insect cells will need to be purified.

There is therefore a continuing need for improvements in 10 protein purification in order to obtain pharmaceutical grade protein derived from recombinant production in insect cells.

OBJECT OF THE INVENTION

It is an object of the invention to provide an improved method for purifying recombinant EGFR family protein expressed in 15 insect cells. It is a further object of the invention to provide an immunogenic variant of HER-2 protein that is usefull in e.g. cancer treatment by means of specific active immunotherapy.

SUMMARY OF THE INVENTION

20 The present inventors have devised a novel method for purifying EGFR family protein to a degree of purity, which is acceptable for pharmaceutical use, notaby for use as vaccine agents.

Hence, in one aspect, the present invention relates to a

. 25 method for purification of an EGFR family derived protein,
said protein being recombinantly produced in an insect cell
culture and said protein being one that is suitable for

4

purification by means of immobilised metal affinity chromatography, the method comprising obtaining, from said insect cell culture, a substantially cell-free sample containing said EGFR family derived protein, and thereafter enriching for said EGFR family derived protein by means of subsequent steps of

- diafiltration and exchange of culture medium with buffer,
- immobilized metal affinity chromatography (IMAC),
- size exclusion chromatography (SEC), and
- 10 anion exchange chromatography (AIE).

Another aspect of the invention relates to an immunogenic variant of HER-2 protein that comprises the amino acid sequence set forth in SEQ ID NO: 2, residues 17-677.

LEGENDS TO THE FIGURE

- 15 Fig. 1: Chromatographic profile of the IMAC.

 The -arrow indicates the 104.1 peak.
 - Fig. 2: Chromatographic profile of the SEC. The arrow indicates the monomer peak.
 - Fig. 3: Chromatographic profile of the AIE.
 - 20 The arrow indicates the 104.1 peak.
 - Fig. 4: The pMT/hHER2MA5-5DUniHis vector p992, plasmid map. hHER2MA5-5D: Gene coding for the hHER2MA5-5DUH protein (nucleotides 3604-5592).
 - P2 epitope: Sequence coding for the P2 epitope in the
 - 25 hHER2MA5-5DUH protein (nucleotides 4357-4401).
 - P30 epitope: Sequence coding for the P30 epitope in the hHER2MA5-5DUH protein (nucleotides 5500-5562).
 - SV40 late Polyadenylation site: Poly A signal (nucleotides

5

263-268).

ColE1: Origin of replication for replication in *E.coli* (nucleotides 701-1434).

Ampicillin resistance gene: Gene conferring ampicillin

5 resistance in bacteria (nucleotides 1579-2439).

Metallothionein promoter: Promoter that can be induced with a number of compounds (e.g. cadmium) (nucleotides 3050-3415).

Kozak like sequence: Ribosomal binding site (nucleotides 3493-3501).

10 BiP signal sequence: Signal sequence directing the HER2 variant protein to secretion into the extracellular compartment (nucleotides 3502-3555).

UniHis sequence: Sequence coding for the UniHis tag used for purification of the HER2 AutoVac protein (nucleotides 3556-

15 3597).

Dipeptidase stop sequence: Used if the UniHis tag is to be cleaved from the HER2 AutoVac protein (nucleotides 3598-3603).

DETAILED DISCLOSURE OF THE INVENTION

In the following a number of term and expressions will be 20 defined in the context of the present invention.

"An EGFR family derived protein" denotes a protein which is homologous to human EGFR (or ErbB-1); human HER-2/neu (ErbB-2); HER-3 (ErbB-3); or HER-4 (ErbB-4).

An "autologous" EGFR family protein is in the present

25 specification and claims intended to denote an EGFR family
polypeptide of an animal that is going to be vaccinated
against its own EGFR family protein. In other words, the term
is only relevant when the relation to the animal that it going
to be vaccinated is considered.

15450DR00

6

The terms "T-lymphocyte" and "T-cell" will be used interchangeably for lymphocytes of thymic origin which are responsible for various cell mediated immune responses as well as
for effector functions such as helper activity in the humeral
immune response. Likewise, the terms "B-lymphocyte" and "Bcell" will be used interchangeably for antibody-producing lymphocytes.

An "antigen presenting cell" (APC) is a cell which presents epitopes to T-cells. Typical antigen-presenting cells are

10 macrophages, dendritic cells and other phagocytizing and pinocytizing cells. It should be noted that B-cells also functions as APCs by presenting T_H epitopes bound to MCH class II molecules to T_H cells but when generally using the term APC in the present specification and claims it is intended to refer to the above-mentioned phagocytizing and pinocytizing cells.

"Helper T-lymphocytes" or " T_H cells" denotes CD4 positive T-cells which provide help to B-cells and cytotoxic T-cells via the recognition of T_H epitopes bound to MHC Class II molecules on antigen presenting cells.

20 The term "cytotoxic T-lymphocyte" (CTL) will be used for CD8 positive T-cells which require the assistance of $T_{\rm H}$ cells in order to become activated.

A "specific" immune response is in the present context intended to denote a polyclonal immune response directed predomi25 nantly against a molecule or a group of quasi-identical molecules or, alternatively, against cells which present CTL epitopes of the molecule or the group of quasi-identical molecules.

7

The term "polypeptide" is in the present context intended to mean both short peptides of from 2 to 10 amino acid residues, oligopeptides of from 11 to 100 amino acid residues, and polypeptides of more than 100 amino acid residues. Furthermore, the term is also intended to include proteins, i.e. functional biomolecules comprising at least one polypeptide; when comprising at least two polypeptides, these may form complexes, be covalently linked, or may be non-covalently linked. The polypeptide(s) in a protein can be glycosylated and/or lipidated and/or comprise prosthetic groups.

The term "subsequence" means any consecutive stretch of at least 3 amino acids or, when relevant, of at least 3 nucleotides, derived directly from a naturally occurring amino acid sequence or nucleic acid sequence, respectively.

15 By the term "down-regulation an autologous EGFR family protein" is herein meant reduction in the living organism of the amount and/or activity of the relevant EGFR family protein. The down-regulation can be obtained by means of several mechanisms including removal of the CEA by scavenger cells (such as macrophages and other phagocytizing cells), and even more important, that cells carrying or harbouring the antigen are killed by CTLs in the animal.

The term "immunogen" is intended to denote a substance capable of inducing an immune response in a certain animal. It will therefore be understood that an autologous EGFR family protein is not an immunogen in the autologous host — it is necessary to use either a strong adjuvant and/or to co-present T helper epitopes with the autologous protein in order to mount an immune response against autologous protein and in such a case the "immunogen" is the composition of matter which is capable of breaking autotolerance.

8

The term "immunogenically effective amount" has its usual meaning in the art, i.e. an amount of an immunogen, which is capable of inducing an immune response which significantly engages pathogenic agents which share immunological features with the immunogen.

The term "pharmaceutically acceptable" has its usual meaning in the art, i.e. it is used for a substance that can be accepted as part of a medicament for human use when treating the disease in question and thus the term effectively excludes the use of highly toxic substances that would worsen rather than improve the treated subject's condition.

A "foreign-T-cell-epitope" is a peptide which is able to bindto an MHC molecule and which stimulates T-cells in an animal species. Preferred foreign epitopes are "promiscuous" epi-15 topes, i.e. epitopes, which binds to a substantial fraction of MHC class II molecules in an animal species or population. A term, which is often used interchangeably in the art, is the term "universal T-cell epitopes" for this kind of epitopes. Only a very limited number of such promiscuous T-cell epitopes 20 are known, and they will be discussed in detail below. It should be noted that in order for the immunogens which are used according to the present invention to be effective in as large a fraction of an animal population as possible, it may be necessary to 1) insert several foreign T-cell epitopes in 25 the same analogue or 2) prepare several analogues wherein each analogue has a different promiscuous epitope inserted. It should be noted that the concept of foreign T-cell epitopes also encompasses use of cryptic T-cell epitopes, i.e. epitopes which are derived from a self-protein and which only exerts 30 immunogenic behaviour when existing in isolated form without being part of the self-protein in question.

9

A "foreign T helper lymphocyte epitope" (a foreign T_R epitope) is a foreign T cell epitope, which binds an MHC Class II molecule and can be presented on the surface of an antigen presenting cell (APC) bound to the MHC Class II molecule. It is also important to add that the "foreignness" feature therefore has two aspects: A foreign T_R epitope is 1) presented in the MHC Class II context by the animal in question and 2) the foreign epitope is not derived from the same polypeptide as the target antigen for the immunization - the epitope is thus also foreign to the target antigen.

A "CTL epitope" is a peptide, which is able to bind to an MHC class I molecule.

The term "adjuvant" has its usual meaning in the art of vaccine technology, i.e. a substance or a composition of matter

15 which is 1) not in itself capable of mounting a specific immune response against the immunogen of the vaccine, but which is 2) nevertheless capable of enhancing the immune response against the immunogen. Or, in other words, vaccination with the adjuvant alone does not provide an immune response against the immunogen, vaccination with the immunogen may or may not give rise to an immune response against the immunogen, but the combined vaccination with immunogen and adjuvant induces an immune response against the immunogen which is stronger than that induced by the immunogen alone.

25 "Diafiltration" is a technique using ultrafiltration membranes to remove salt or solvent, exchange buffers, or fractionate different size biomolecules in macromolecular solutions. Macromolecules retained by the ultrafiltration membrane are concentrated while solvent and low molecular weight species are removed. However, a simple concentration of the macromolecular sample will not completely remove the smaller

10

species. Therefore, the smaller species must be "washed" from the sample using multiple wash volumes (diafiltration). After the diafiltration process, the sample can be concentrated for further analysis or purification. This is an advantage compared with gel filtration or dialysis when the sample can be diluted during the separation process, requiring an additional concentration step. There is no loss or contamination using diafiltration as could occur with a two-step process.

- 10 "Immobilised metal affinity chromatography" (IMAC) is a chromatographic technique where proteins are purified as a consequence of their affinity for certain divalent metal ions, cf. the descriptione in the "Background of the Invention".
- "Size exclusion chromatography" is a chromatographic

 15 technique, where proteins and other macromolecules are
 fractionated according to their physical size. Small molecules
 are retained in pores of the matrix and are therefore cluted
 slowly, whereas larger molecules are excluded and therefore
 eluted early from the matrix.
- 20 "Anion Exchange Chromatography" is a chromatographic technique, where molecules having a net negative charge are retained on the column matrix and subsequently eluted by displacing with anion from the elution buffer.

Description of the preferred embodiments

25 The present invention relates to a purification process that is especially tailored for purification of EGFR family derived proteins that have been produced recombinantly in insect cells. The present invention was conceived in connection with efforts that has led to the preparation of immunogenic

15450DR00

11

variants of the human cancer-associated antigen HER-2 - these variants are produced in the DES® expression system, an expression system owned by GlaxoSmithKline and marketed by i.a. Invitrogen. The system utilises S2 Drosophila cells and specialised vectors. The use of S2 cells as host cells for recombinant production has, however, posed its own set of problems to solve vis-à-vis the HER-2 variant in question, and these problems have been solved by using the inventive method (i.a. problems with co-migrating proteins which are derived from the S2 cells).

The particular protein that is used in the Examples is a variant of human HER-2, which is immunogenic in humans - the variant includes the amino acid sequence set forth in SEQ ID NO: 2, residues 17-677. However, since this amino acid sequence is not in itself suitable for IMAC, it contains an N-terminal histidine tag (amino acid residues 1-14 in SEQ ID NO: 1) that can be cleaved off by an aminodipeptidase (dipeptidyl peptidase I, DPPI, cf. Pedersen J et al., 1999, Protein Expression and Purification 15, 389-400). The stop sequence 20 for the diaminopeptidase consists of residues 15 and 16 in SEQ ID NO: 2.

Therefore, in general the instant purification method is especially suited for EGFR family derived proteins that include a heterologous amino acid sequence that facilitates

25 purification by means of IMAC. This sequence may be native to the EGFR family derived protein, but more often it is heterologous amino acid sequence (i.e. not naturally associated with the EGFR family derived protein). Preferred amino acid sequences for this purpose are rich in histidine

30 residues (e.g. the His, tag and other amino acid sequences with several consecutive histidine residues). The most preferred heterologous amino acid sequence that facilitates IMAC

15450DR00

12

purification is the one comprising residues 1-14 of SEQ ID NO: 2.

The EGFR derived protein subjected to the inventive process is preferably one that comprises a substantial part of the amino 5 acid sequence of human EGFR or human HER-2, and it is especially preferred the this substantial part is mainly derived from the extracellular portion of human EGFR or human HER-2. Most preferred is a variant of human HER-2, and in the most preferred embodiments, the variant of human HER-2 includes at least one foreign T helper cell epitope.

As mentioned above, the inventive process has been conceived in connection with work on recombinant production of certain variants of human HER-2 antigen. These variants are characteristic in including promiscuous foreign T-helper 15 epitopes that are introduced into the amino acid sequence of human HER-2 extracellular domain. Preferred variants of human HER-2 include tetanus toxoid epitopes P2 (residues 269-282 of SEQ ID NO: 2) and P30 (residues 649-669 of SEQ ID NO: 2) and the most preferred variant has an amino acid sequence that 20 consists of residues 1-677 of SEQ ID NO: 2

Diafiltration/buffer exchange

The step of diafiltration/buffer exchange is performed at a temperature from about 2 to about 25°C. However, preferably temperatures in the lower part of the range are used, e.g.

25 temperatures below 20°C, such as below 15°C or below 10°C. Most preferred temperatures are in the range between 2 and 9°C, such as in the range between about 3°C and about 9°C, with a most preferred temperature range from about 4 to about 6°C. At higher temperatures (e.g. beyond 10°C) there is a tendency that

15450DX00

13

the protein aggregates, and this can be counteracted by adding a detergent, such as a Tween type detergent.

Normally, the diafiltration is performed in two rounds so as to initially concentrate macromolecular compounds in the 5 sample of culture medium and thereafter to exchange culture medium with buffer. These procedures are done following standard procedures in the art, cf. also the examples. It is preferred that the concentration step results in a concentration of between 2 and 25 times of the macromolecular compounds, such as a concentration between 2 and 20 times, 3 and 15 times, between 3 and 10 times. Preferred concentration of macromolecular compounds is in the range of between 4 and 8 times, and the most preferred concentration is about 5 times.

The buffer exchange is typically performed in two subsequent steps of which the first takes place at a pH of at least 6.5 and at most 7.2 and of which the second takes place at a pH of at least 7.0 and of most 8.0. It is, however, possible to perform both steps at the same pH in the overlapping part of the two ranges. Typically, the buffer exchange is performed using a phosphate buffer.

After completion of the buffer exchange, the stringency of the following steps is preferably increased by adding an agent to the sample that will compete for binding to the chromatographic matrix in the IMAC step so as to reduce the 25 amount of non-significant binding by contaminating constituents. For example, addition of imidazole, histidine or a high salt concentration buffer to the diafiltrated and buffer can be done to increase the stringency. Preferably, imidazole is added so as to reach a concentration in the range 30 between about 0.05 to about 20 mM, preferably in the range from about 0.5 to about 15 mM, such as in the range from about

15450DR00

14

1 to about 10 mM. Especially preferred is concentration of imidazole in the range from about 2 to about 9 mM, such as a concentration from about 3 to about 8 mM. most preferred is an imidazole concentration of about 4 to about 6 mM, such as a concentration about 5 mM. When using a high salt concentration buffer (often NaCl), the concentration is in the range from 100 mM up to about 1 M.

It is also preferred to add a detergent to the diafiltrated and buffer changed sample prior to the IMAC step. The 10 detergent will normally be selected from a polyoxyethylene sorbitan fatty acid ester such as Tween 20, Tween 40, Tween 60, Tween 80, and Tween 85, an alkylaryl polyether alcohol

such as Triton X100, a non-ionic detergent, and a carbohydrate based detergent such as octylglycoside. The detergent is advantageously added to reach a concentration of between about 0.05% (v/v) and 10% (v/v), such as about 0.1% (v/v).

IMAC

The IMAC step involves charging of a chromatographic medium with a divalent metal ion prior to application of the buffer 20 exchanged sample thereto. Typically, the divalent metal ion is selected from the group consisting of Ni²⁺, Cu²⁺, Zn²⁺, Co²⁺, and Fe²⁺. Preferably, the divalent metal ion is Zn²⁺.

Elution of the chromatographic medium in the IMAC is performed by applying imidazole, histidine, a high salt concentration 25 buffer, or a change of pH onto the chromatographic medium (typically in a chromatograpic column). For instance, when using imidazole for elution, this is advantageously done by applying the imidazole in one single step at a concentration between about 50 mM and about 500 mM (such as between 100 and 400 mM), preferably at a concentration of about 200 mM.

15450DX00

15

Alternatively, when histidine is used this is done by applying the histidine in one single step at a concentration between about 20 mM and 400 mM (such as between 50 and 200 mM), preferably about 100 mM. The high salt concentration buffer 5 usually contains NaCl in conctrations up to about 1 or even 2 M.

SEC

The average pore size of the SEC matrix is preferably one that separates globular protein between 10 kDa and 600 kDa.

- 10 After having applied the sample to the matrix, elution is done with a phosphate or TRIS buffer or, alternatively, with a biological buffer such as HEPES. It has surprisingly been found that phosphate buffers are suitable for the following AIE step, something which is normally considered

 15 disadvantageous but the present inventors have encountered no
- 15 disadvantageous but the present inventors have encountered no problems in this respect.

pH is maintained in the range of about 7 to about 8 during the SEC and preferably the pH is kept about 7.5.

If relevant and necessary (i.e. when a phosphate buffer is
20 used in the SEC step), samples containing the EGFR family
derived protein obtained from SEC, is diluted before the AIE
step so as to adjust the phosphate concentration to less than
15 mM, such as to the range between 10 and 12.5 mM. However,
it is, as mentioned above, surprising that the AIE can be
25 performed using such a phosphate buffer concentration.

AIE

The final step in the purification procedure of the invention is an AIE step. This step preferably involves loading of the

16

sample containing the EGFR family derived protein obtained after SEC on a strong or weak anion exchange matrix.

Typically, the elution is performed with a buffered (phosphate, TRIS or a biological buffer such as HEPES) NaCl solution at a pH between 7 and 8, preferably about pH 7.5.

The protein obtained in the eluate after these four steps has a clinical grade purity and is substantially free of contaminants derived from the insect cell culture.

HER-2 variant of the invention

- As mentioned above, the present inventive method has been conceived when purifying a variant of the human HER-2 tumour antigen. This particular variant has proven to be especially well-suited as a vaccine agent for inducing immunological reactions against autologous HER-2 so this particular variant is also a part of the present invention.
- In general, the specific use, formulation, recombinant production, suitable vectors and host cells as well as other details pertaning to this specific HER-2 variant can be found in the disclosure of WO 00/20027. Hence, in the following only 20 a brief discussion will be provided that specifically pertains to the variant. Hence, the disclosure of WO 00/20027 is included by reference herein and provides for the necessary teachings concerning immunization with HER-2 variants and the general methods for producing these and their formulation.
 - 25 Also the disclosure in WO 00/20027 relating to nucleic acid vaccination against autologous HER-2 is incorporated by reference herein.

As mentioned above, another aspect of the present invention relates to an immunogenic variant of HER-2 protein that

17

comprises the amino acid sequence set forth in SEQ ID NO: 2, residues 17-677. It is preferred that this variant is a polypeptide that consists of the amino acid sequence set forth in SEQ ID NO: 2, residues 1-677, i.e. a variant that also includes a histidinyl-rich purification tag consisting of residues 1-14 in SEQ ID NO: 2, and an aminopeptidase stop sequence consisting of residues 15 and 16 in SEQ ID NO: 2.

Also included in the present invention is a nucleic acid fragment that encodes this immunogenic variant of HER-2

10 protein, such as a DNA fragment. An especially preferred DNA fragment has the HER-2 variant encoding sequence set forth in SEQ ID NO: 1.

Useful tools in the recombinant production of HER-2 variants are vectors carrying the nucleic acid fragment of the invention. Especially preferred is a vector capable of autonomous replication. Typically, the vector is selected from the group consisting of a plasmid, a phage, a cosmid, a minichromosome, and a virus.

Expression vectors are especially preferred. A typical
20 expression vector of the invention comprises, in the 5'→3'
direction and in operable linkage, a promoter for driving
expression of the nucleic acid fragment of the invention,
optionally a nucleic acid sequence encoding a leader peptide
enabling secretion of or integration into the membrane of the
25 polypeptide fragment, the nucleic acid fragment of the
invention, and optionally a nucleic acid sequence encoding a
terminator.

For recombinant production, a host cell transformed with the vector of the invention is especially preferred. A 30 particularly interesting host cell is an insect cell, and most

18

preferred is a drosophila derived host cell such as an S2 cell.

Also part of the inventin is a stable cell line which carries the vector of the invention and which expresses the nucleic 5 acid fragment of the invention, and which optionally secretes or carries on its surface the immunogenic variant of HER-2 protein of the invention.

Furthermore, the invention also provides for an immunogenic composition for immunizing against HER-2 protein in a human comprising the immunogenic variant of HER-2 protein described above in admixture with a pharmaceutically acceptable carrier or vehicle and optionally an adjuvant. Details on suitable formulations can be found in WO 00/20027.

Alternatively, the vaccine may be in the form of a nucleic acid vaccine (for details concerning this technology, cf. WO 00/20027). Thus, also part of the invention is an immunogenic composition for immunizing against HER-2 protein in a human comprising the vector described above in admixture with a pharmaceutically acceptable carrier or vehicle and optionally an adjuvant

Also embraced by the scope of the present invention is a method for immunizing a human against autologous HER-2, the method comprising administering, to the human being, an immunogenically effective amount of

- 25 the immunogenic variant of HER-2 protein described herein or an immunogenic composition comprising the variant, or
 - the vector described herein or an immunogenic composition comprising said vector.

15450DR00

19

It is especially preferred that this immunization method (as well as the different means for immunization described herein) is used for treating or ameliorating cancer.

PREAMBLE TO THE EXAMPLES

5 The following exemplification utilizes the "104.1 molecule" (cf. SEQ ID NO: 2) which is an immunogenic analogue of the cancer associated HER-2 protein. However, it will be understood by the person skilled in the art that the general teachings of the present invention are applicable for other 10 His tagged proteins, especially those produced recombinantly in insect cell systems.

The purification process consist of the following 4 general steps:

- Diafiltration with buffer change of fermentation
 supernatant.
 - 2. Immobilized Metal Affinity Chromatography (IMAC)
 - 3. Gelfiltration/Size Exclusion Chromatography (SEC)
 - 4. Anion Exchange Chromatography (AIE)

Diafiltration/buffer exchange

- 20 The diafiltration serves three purposes 1) to concentrate the substance "104.1" 2) to remove low molecular weight substances from the fermentation medium that could interfere with the subsequent capture step, such as metal ions and 3) to change buffer into a buffer more suitable for metal chelate
- 25 chromatography (IMAC). Buffer exchange takes place in two

154500R00

20

steps, first into 50 mM phosphate buffer pH 7.0 and then into 50 mM phosphate buffer pH 7.5. This pH sequence seems to be critical because going directly into pH 7.5 leads to precipitation of not identified components from the 5 fermentation medium, when the fermentation medium is insect cell medium. Concentration is mainly performed to reduce loading time in the subsequent IMAC and to reduce consumption of buffer in the buffer exchange step and is not found essential for the process, as the subsequent IMAC by nature is a concentrating process step. The concentration scale is described to be 5 times but experiments using 10 times concentration also seem to work and it is expected that it is possible to go higher, such as 20 or even 25 times. Further

concentration than the 5 times described in the protocol may 15 improve the process, as it would decrease the loading time on the following IMAC column.

Sample preparation for IMAC .

The diafiltrate is prior to application to the IMAC column prepared by adding imidazole to a final concentration of 0-10 20 mM. If no imidazole (or a similar substance) is added, we have experienced co-purification of other proteins from the insect cells with 104.1. Furthermore, Tween 20 is added (after filtration) to a final concentration of 0.1% (v/v). Up to 5% can be applied for the IMAC step and higher concentration than 25 0.1% will lead to less dimer formation. Other detergents are also expected to be useful, obviously other Tweens (Tween 40, 60, 80 and 85).

IMAC

The substance 104.1 has a so-called His-tag in the N-terminus 30 that has affinity for complexed divalent metal ions

21

immobilized on the column matrix. Critical parameters are choice of divalent metal ion and choice of elution agent/method. Ni²⁺, Cu²⁺ and Zn²⁺ can all be used as the chelating metal ion. However, Zn²⁺ has provided superior recovery and fewer impurities. For elution of captured 104.1 several strategies can be used. 1) Application of imidazole to the column 2) application of histidine to the column 3) application of high salt concentration buffer to the column and 4) change of pH on the column.

10 The described process uses elution by application of 200 mM imidazole in one step. However, down to 50 mM can be used but the result is less concentrated 104.1 and lower recovery.

SEC

The example below describes that the SEC is run in phosphate

15 buffer. However, TRIS seems to work as well and TRIS is more
suitable for the following AIE than phosphate. The current
protocol describes dilution of the SEC eluate before
application on the AIE column in order to reduce the phosphate
concentration, and this will not be necessary with TRIS. It is

20 nevertheless surprising the a phosphate buffer can be used at
all.

If the IMAC was run in Tween-20 concentration higher than 0.4%, it should be adjusted to < 0.4% in the SEC, as the 104.1 protein does not bind to the AIE column if the concentration of Tween-20 is higher than 0.1%. This may be different if the AIE is run in TRIS instead of phosphate.

Sample preparation for AIE Chromatography

The relevant fractions from SEC are diluted in water, 1 volume eluate + 3 water, to reduce the phosphate concentration as it

22

interferes with the AIE chromatography. This issue is also discussed in the SEC paragraph.

AIE Chromatography

The critical parameters are the pH and ionic strength of the 5 sample and buffer systems.

If the SEC was run in TRIS the sample preparation (dilution in water) could be avoided and the loading volume (and loading time) would be reduced.

Final bulk product is analysed by SDS-PAGE, western blotting

10 (WB), ELISA, HPLC, visual inspection, OD₂₈₀, pH, Limulus

Amoebocyt Lysate (LAL) and amino acid analysis. Intermediate products are analysed by SDS-PAGE, WB, ELISA and OD₂₈₀.

EXAMPLE 1

Culturing of HER-2 variant 104.1

15 Cell line production

A polyclonal culture of \$2 Drosophila melanogaster cells was transfected with a pMT vector (DES® system, Invitrogen) containing the gene coding for the HER2 variant 104.1; the entire nucleic acid sequence of this pMT vector is set forth 20 in SEQ ID NO: 1. The cells were in parallel transfected with a plasmid carrying a gene conferring hygromycin resistance enabling the usage of hygromycin for selection of transfected cells.

154500K00

23

A limited dilution technique was used for isolation of single cell clones and a Master Cell Bank (MCB) was produced from the selected cell line.

HER2 protein AutoVac production

- 5 One vial from the MCB is resuscitated in a T-flask and propagated in shake flasks containing ExCell420 media (JRH) at 25°C to obtain enough biomass for the inoculation of a bioreactor. A total of 45x10° cells is diluted into 3000 mL with ExCell 420 supplemented with 4 mM Glutamine, 0.1%
- 10 Pluronic F68, and 0.5 mL/L PD30 antifoam. The 3000 mL are used to inoculate an Applikon bioreactor (7 L working volume)

 where the culture grows for 3 days at 25°C, d02 = 50% (100% = air saturation), pH = 6.5 ± 0.1 (adjusted with 5 % H₃PO₄ and 0.5 M NaOH), and stirred at 170 rpm.
- 15 This culture is diluted with ExCell 420 supplemented with 4 mM Glutamine, 0.1% Pluronic F68, and 0.5 mL/L PD30 antifoam to a total cell concentration of 15 x 10⁶ cells/mL and used for inoculation of a 15 L working volume Applikon Bioreactor maintaining 25°C, dO₂ = 50 % (sparging with pure oxygen), pH =
- 20 6.5 ± 0.1 (adjusted with 5 % H₃PO₄ and 0.5 M NaOH), and stirred at 142 rpm. The culture is continuously diluted with ExCell 420 supplemented with 4 mM Glutamine and 0.1 % Pluronic F68 until a total volume of 10 L is reached. The dilution rate is adjusted daily to prevent the cell number to drop below 15 x
- 25 10⁶ cells/mL. PD30 antifoam iss added manually to the culture to maintain a total concentration of 0.5 mL/L.

When filling is completed, perfusion is initiated at 1 RV/day (reactor volumes per day) using the BioSep cell (AppliSens) acoustic retention device to prevent cell loss with the

30 removed media. At a cell concentration of 30 x 10⁶ cells/mL,

15450DR00

. 24

the culture is induced by addition of a total of 2 μM CdCl₂ (10 mM stock) to the culture and to the medium reservoir.

The fermentation medium is harvested, centrifuged to obtain a cell free supernatant, and filtrated through a PALL filter 5 0.8/0.22 µm. The resulting sterile supernatant is either stored at -80°C until use (storage up to three months at -80°C has not produced detectable stability problems) or stored at 4°C without for up to one week (also without any detectable degradation of the protein).

10 The culture is terminated 10 days post induction and the residual culture media in the bioreactor is discarded.

EXAMPLE 2

Diafiltration/Concentration and Buffer Change

Before use, the fermentation supernatant from Example 1 is, if 15 kept at -80°C, thawed slowly at 4°C over night (the last 3 to 4 hours in cold water), and thereafter stored for a maximum of 1 day at 4°C. Otherwise, the fermentation supernatant is used directly.

The fermentation supernatant is centrifuged in a Sorvall RE 5C 20 Plus Centrifuge in SCA3000 tubes at 10,000 rpm for 15 min, at 4°C.

Diafiltration is performed in a cold room at $4-6^{\circ}\text{C}$ on a ProFlux M12 (Millipore) with a Pellicon 2 Casette filter 30K 0.5 m² (Millipore, Cat# P2B030A05). The filter is before use stored

25 in 0.1 M NaOH. Before diafiltration the filter is therefore thoroughly washed through with milli-Q water: The standard

25

reservoir is filled with milli-Q water (3L) and washed with water through the filter until 200 ml is left in the reservoir. This procedure is repeated 3 times until a total of 12 litres has passed through the filter. Now, diafiltration 5 can be instigated:

A maximum of 15 L fermentation supernatant is concentrated 5 times: The recirculation pump is started. The backpressure valve should be partly locked, to give an outlet pressure that shows back pressure (e.g. 0.2 bar). The pump speed is adjusted 10 to 30-50%. The pressure difference should show 0.7 - 1.2 Bar, as this is when the filter's maximum capacity is used and flow over filter correspond to 3-4 L/min (e.g. Outlet P=0.2 Bar,

Inlet P=1.0 bar, Δ P=0.8). Inlet pressure should show max 1.4 bar considering tubing life and performance. If a higher inlet pressure is desired, the recirculation pump pressure can be elevated (%) or the mechanical pressure on the tubing could be elevated by applying higher pressure on the tubing (scale 0-5). When the back pressure valve is closed, a higher inlet and higher outlet pressure is received. The back pressure valve should never be completely shut.

Subsequently, the concentrated fermentation supernatant is subjected to buffer exchange, first using 10 volumes 50 mM Na₂HPO₄/NaH₂PO₄, pH 7.0, and then by 10 volumes 50 mM Na₂HPO₄/NaH₂PO₄, pH 7.5: The standard reservoir on the ProFlux 25 M12 Millipore apparatus is filled with buffer to a total volume of 3L and also the side reservoir is filled with buffer. The setting on the apparatus is the same as when concentrating the sample.

The volume of the buffer changed sample (Vb) is measured and a 30 a sample is taken out for SDS-PAGE (Sb). The concentrated

26

buffer changed sample is portioned into 11 ml and 50 ml lots and frozen quickly to -80 °C.

Analysis of the Diafiltrate

pH and ionic strength is measured to assure efficiency of the 5 buffer exchange.

Total protein concentration is estimated spectrophotometrically at 280 nm in a 1 cm cuvette. A 10 times diluted sample (dilute in 50 mM sodiumphosphate buffer pH 7.5) with 50 mM sodium phosphate buffer pH 7.5 is used as reference (using the approximation Abs₂₈₀ of 1 = 1 mg/ml total protein). The specific concentration of variant 104.1 is measured by ELISA and the diafiltrate is furthermore analysed by SDS-PAGE, silver stained and WB-ECL detection.

Remarks to the Diafiltration Step

15 It is important to start the buffer exchange at pH 7.0 before changing to pH 7.5. Otherwise, residual components from the fermentation medium precipitate.

Diafiltered samples have been stored at -80 °C for several months without change in performance in the quantitative HER-2 20 ELISA. However, when thawed, even short exposure to 37 °C and 54 °C dramatically decreases the performance of the diafiltrate in the same ELISA. When kept at 0 °C (ice/water) and 4 °C after thawing from -80 °C, the performance in the ELISA of the diafiltrate is stable for up to at least 4 hours.

25 EXAMPLE 3

15450PX00

27

IMAC

The general chromatographic principle for IMAC is affinity between a "tag" on the protein and a metal ion chelate complex on the column matrix. The chromatographic matrix is POROS 20MC 5 (Applied Biosystems) and the chelating metal ion is Zn²⁺. The 104.1 molecule is provided with a His-tag and the buffer system for binding of the His-tag to the column matrix is 50 mM Na₂HPO₄/NaH₂PO₄, 5 mM Imidazol, 0.1 % Tween20, pH 7.5. Three mg 104.1 per ml column material is loaded and subsequently eluted using 200 mM Imidazol, 50 mM Na₂HPO₄/NaH₂PO₄, pH 7.5, 0.1 % Tween20.

-Instrument: VISION-Work-Station-(Applied-Biosystems) -

Software: Data analysis software for Vision, BioCAD 700E,

version 3 series software, Perseptive Biosystem.

15 **Detection:** UV absorbance at $\lambda = 280$ and 220 nm.

Conductivity: 0 - 200 mS

pH calibrated at: 7.0 and 10

Temperature: The procedure was made with buffers and column at room temperature (20-24°C) and loading of sample on ice and

20 fraction collection at 10°C.

Sample Preparation

To the diafiltrate containing the 104.1 molecule, 800 mM imidazole is added to a final concentration of 5 mM imidazole. Immediately before application to the column the sample is filtrated by vacuum through OSMONICS AcetatePlus, Supported, plain, 0.22 µm filter, (cat# A02SP04700) and Tween20 is added to a final concentration of 0.1% (v/v). The sample is kept at 4°C until application to the column where it is held on ice when applied. Handling time at room temperature should be 30 minimized.

15450DR00

28

Column

POROS 20 MC in a 16 \times 100 mm (20.1 ml) PEEK column (Applied Biosystems) packed at 2000-2500 psi.

Buffer Stocks

5 Buffer A: 250 mM Na₂HPO₄/NaH₂PO₄, pH 7.5, 0.5 % Tween20

Buffer B: H₂O (Milli-Q)

Buffer C: 12.5 mM Imidazol, pH 7.0

Buffer D: 800 mM Imidazol, pH 7.0

Buffer E: 0.1 M EDTA, 1 M NaCl, pH 4.2

10 Buffer F: 100 mM ZnCl2, pH 4.5/ Sample

Column Charge (strip-charge) Program

Flow: 10 ml/min.

- 1. 20 CV Buffer E (strip)
- 2. 20 CV Buffer B
- 15 3. 40 CV Buffer F
 - 4. 40 CV Buffer B

The column should be charged before each run.

Chromatography Program

20 Flow rate 30 ml/min, loading 5 ml/min.

Fraction collection size 9 ml, and 5 ml at elution peak 200 mM imidazole. Collect in a cooled (10°C) fraction collector.

- Purge system 20 ml (30 ml/min)
- 2. Equilibration: 20 CV 40 % buffer C, 20% buffer A
- 25 3. Load: sample through pump, 5 ml/min.

5

29

- 4. Wash: 40 CV 40 % buffer C and 20% buffer A
- 5. Elution:
 - 10 CV 25 % buffer D, 20% buffer A
 - 5 CV 50 % buffer D, 20% buffer A
 - 5 CV 80 % buffer D, 20% buffer A
- 6. Wash: 20 CV buffer B (H2O)

Pool the fractions from the eluted peak from chromatogram (cf. Fig. 1). Begin pooling at peak start and collect a total of 50 ml or pool fractions based on SDS-PAGE/WB results or ELISA to a total of 50 ml. This pool can be saved over night at 4°C or carried on to SEC straight away. Storage of pool up 7 days at 4°C, -20°C and -80°C has shown no loss in total protein after

filtration through 0.22 μm filter when analysed on SDS PAGE and 15 WB-ECL.

Sanitization of column

Wash the column with 5 CV 1 M NaOH, 2 M NaCl, followed by 10 CV of water. If further sanitization is needed see the RSP from the manufacturer. The column is stored in 30% EtOH at 5-20 30°C.

Analysis of IMAC Intermediate

Start material, flow through and eluted fractions are analysed by WB-ECL and SDS-PAGE/silver stained.

Analysis of IMAC Pool

25 The pool is analyzed by WB-ECL and SDS-PAGE/silver stained, HPLC and $OD_{280\ nm}$ (on 10 times diluted sample). The specific 104.1 concentration is determined by ELISA.

15450DX00

30

EXAMPLE 4

SEC Gel Filtration Chromatography

The gelfiltration step is run in 50 mM Na₂HPO₄/NaH₂PO₄, 0.1% Tween20, pH 7.5. Fifty ml from IMAC of Example 3 is loaded by 5 Superloop (Pharmacia) on a Superdex 200 prep grade matrix.

Instrument: BioCAD 700E Work Station for Perfusion Chromatography equipped with a semi-preparative flow cell to reduce the back pressure on the column.

Software: Data analysis software for Vision, BioCAD 700E,

10 version 3 series software, Perseptive Biosystem.

Detection: UV absorbance at λ = 280 and 220 nm.

Conductivity: 0 - 200 mS

pH calibrated at: 7.0 and 10

Temperature: Buffers and column are room temperature (20-24°C)

15 and the sample is loaded directly from 4°C. Fractions containing the monomer 104.1 should be moved to 4°C directly after collection if the collector is not cooled.

Sample Preparation

The Pool from IMAC in buffer, 50 mM Na₂HPO₄/NaH₂PO₄, 0.1% 20 Tween20, 200 mM imidazol, pH 7.5, requires no special preparation. The sample should be kept cool (4-6°C) until loading.

Column

Superdex 200 prep grade, packed in Pharmacia column XK 25 50x960mm (1884 ml) at 15 ml/min as final flow rate. Load maximum 50 ml.

31

Buffer Stocks

Buffer A: 250 mM Na₂HPO₄/NaH₂PO₄, pH 7.5, 0.5 % Tween20

Buffer B: H₂O

Chromatography Program

5 General flow rate 8 ml/min, load 5 ml/min.

Fraction size 9.0 ml

- 1. Equilibration 1.5 CV 20% buffer A (see remarks)
- 2. Load: via 50 ml Super Loop, 5 ml/min
- 3. Elution 1.2 CV 20% buffer A

The fractions from the monomer peak (cf. Fig. 2) are pooled by comparing gel results to obtain a pure product (approximately 130 ml). This pool can be saved over night at 4°C or carried on directly to the AIE chromatography of Example 5. Storage of 15 pool up to 7 days at 4°C, -20°C and -80°C has shown no loss in total protein after filtration through 0.22 µm filter when analysed by SDS PAGE and WB-ECL.

Sanitization and cleaning of column

The column is cleaned by running 0.5 NaOH in the reversed flow direction for 1-2 h at 6.5 ml/min (20 cm/h) followed by 3 bed volumes of buffer. For sanitization run 0.5-1.0 NaOH in reversed flow direction, 13 ml/min (40 cm/h) for 30-60 min followed by 3-5 bed volumes of sterile buffer. The column is stored in 20% ethanol at 4-8°C. For additional information 25 confer manufactures manual.

15450DX00

32

Analysis of the SEC Intermediate

Start material and eluted fractions are analyzed by WB-ECL and SDS-PAGE/silver stained.

Analysis of SEC Pool

5 The pool is analysed by WB-ECL and SDS-PAGE/silver stained, HPLC and $OD_{280\ nm}$. The specific 104.1 concentration is determined by ELISA.

Remarks to SEC

Make sure that the sample is kept at 4°C between IMAC and 10 loading from the Superloop.

If the fraction collector is not cooled (10°C) make sure that fractions are moved to cold room/fridge immediately after the collection.

When the column is frequently used, a constant flow (0.2 15 ml/min) of 50 mM Na₂HPO₄/NaH₂PO₄, pH 7.5, 0.5% Tween 20 is applied to the column.

EXAMPLE 5

AIE Chromatography

Anion exchange chromatography is performed at pH 7.5 (20 mM 20 TRIS), preferably on a strong anion exchange perfusion matrix POROS 50HQ (Applied Biosystems) in a PEEK 4.6x100 mm (1.662 ml) column. 104.1 is eluted in 200 mM NaCl.

Instrument: VISION Work Station for Perfusion Chromatography.
Software: Data analysis software for Vision, BioCAD 700E,

33

version 3 series software, Perseptive Biosystem.

Detection: UV absorbance at $\lambda = 280$ and 220 nm.

Conductivity: 0 - 200 mS

pH calibrated at: 7.0 and 10

5 Temperature: The procedure was made with buffers and column at room temperature (20-24°C) and loading of sample from ice. The fraction collector was cooled to 10°C.

Sample Preparation

The SEC intermediate is diluted 1+3 (to 25%) in water

10 containing 0.1% Tween20 under gentle magnetic stirring. The

sample should be kept cool (4-6°C) until and during loading.

Column

POROS 50HQ is packed in a 4.6×100 mm (1.662 ml) PEEK column (Applied Biosystems) at 2000-2500 psi.

15 Buffer Stocks

Buffer A: 100 mM TRIS, 0.5% Tween20, pH 7.5

Buffer B: H2O

Buffer C: 2 M NaCl

Buffer D: 2 M NaOH, 1 M NaCl

20 Buffer E: 100 mm NaCl

Buffer F: Sample

Chromatography Program

General flow rate 10 ml/min, load sample 5 ml/min.

25 Fraction size: 9 ml during sample load, 1 ml during 1st elution step, and 5 ml during 2nd elution step

34

- Purge System 20 ml (20 ml/min)
- 2. Equilibration: 20 CV 20% buffer A
- 3. Load sample via pump (5 ml/min)
- 4. Wash: 10 CV wash in 20% buffer A
- 5 S. Wash: 10 CV wash in 20% buffer A, 20% buffer E
 - 6. Elution:
 - 20 CV 20% buffer A, 10% buffer C
 - 10 CV 20% buffer A, 50% buffer C
- 10 The fractions from the elution peak (cf. Fig. 3) are pooled by comparing gel results to obtain a concentration of more than 1 mg/ml or OD_{280nm} more than 1.0. The fractions can be kept over night at 4°C before pooled. Storage of pool up to 7 days at 4°C, -20°C and -80°C has shown no loss in total protein after
- 15 filtration through 0.22 μm filter when analysed by SDS PAGE and WB-ECL.

Sanitization of column

Wash the column with 10 column volumes (CV) of 1 M NaOH, 2 M NaCl, followed by 20 CV of water. If further sanitization is 20 needed confer manufacturer's manual. The column is stored in 30% ethanol at 5-30°C.

Analysis

Start material, flow through and eluted fractions are analysed by WB-ECL and SDS-PAGE/silver stained.

25 Analysis of AIE Pool

The pool is analysed by WB-ECL and SDS-PAGE/silver stained, Appearance and description, pH, HPLC, LAL and $OD_{280\ nm}$ (use 3

35

times diluted sample). The specific 104.1 concentration is determined by ELISA.

Remarks to AIE

If the SEC intermediate is diluted less than 1 + 3 (25%) 104.1 5 is detected in the run-through from the AIE due to interference from the phosphate buffer.

Up to 25 mg 104.1 has been applied to the AIE column without detectable amounts of 104.1 in the run-through.

Storage of Final Bulk Product

10 The final bulk product is stored at -80°C in a polypropylene container after filtration through 0.22 µm filter.

The product thus obtained has a purity which is suitable for clinical use.

15450DK0D

36

Modtaget PVS 25 JUNI 2003

CLAIMS

- 1. A method for purification of an EGFR family derived protein, said protein being recombinantly produced in an insect cell culture and said protein being one that is suitable for purification by means of immobilised metal
- 5 suitable for purification by means of immobilised metal affinity chromatography, the method comprising obtaining, from said insect cell culture, a substantially cell-free sample containing said EGFR family derived protein, and thereafter enriching for said EGFR family derived protein by means of
- 10 subsequent steps of
 - diafiltration and exchange of culture medium with buffer,
 - .m immobilized metal affinity chromatography (IMAC),
 - size exclusion chromatography (SEC), and
 - anion exchange chromatography (AIE).
- 15 2. The method of claim 1, wherein the EGFR family derived protein includes a heterologous amino acid sequence that facilitates purification by means of IMAC.
 - 3. The method of claim 2, wherein the heterologous amino acid sequence is rich in histidine residues.
- 20 4. The method according to claim 3, wherein the heterologous amino acid sequence comprises residues 1-14 of SEQ ID NO: 2.
- 5. The method according to any one of the preceding claims, wherein the EGFR family derived protein comprises a substantial part of the amino acid sequence of human EGFR or 25 human HER-2.
 - 6. The method according to claim 5, wherein the substantial portion is mainly derived from the extracellular portion of EGFR or HER-2.

37

- 7. The method according to claim 5 or 6, wherein the EGFR family derived protein is a variant of human HER-2.
- 8. The method according to claim 7, wherein the variant of human HER-2 includes at least one foreign T helper cell5 epitope.
 - 9. The method according to claim 8, wherein the variant of human HER-2 includes tetanus toxoid epitopes P2 (residues 269-282 of SEQ ID NO: 2) and P30 (residues 649-669 of SEQ ID NO: 2).
- 10 10. The method according to claim 9, wherein the variant of human HER-2 includes amino acid residues 17-677 of SEQ ID NO: 2.
- 11. The method according to claim 10, wherein the amino acid sequence of the variant of human HER-2 consists of residues 1-15 677 of SEQ ID NO: 2.
- 12. The method according to any one of the preceding claims, wherein the step of diafiltration/buffer exchange is performed at a temperature from about 2 to about 25°C, preferably at a temperature of about 4 to about 6°C, optionally with the 20 addition of a detergent such as Tween when the temperature is beyond 10°C.
- 13. The method according to claim 12, wherein the diafiltration is performed in two rounds so as to initially concentrate macromolecular compounds in the sample of culture 25 medium and thereafter to exchange culture medium with buffer.

38

- 14. The method according to claim 13, wherein the macromolecular compounds are concentrated between about 2 and about 25 times.
- 15. The method according to claim 14, wherein the5 macromolecular compounds are concentrated about 5 times.
- 16. The method according to any one of claims 12-15, wherein the buffer exchange is performed in two subsequent steps of which the first takes place at a pH of at least 6.5 and at most 7.2 and of which the second takes place at a pH of at 10 least 7.0 and of most 8.0.
 - 17. The method according to any one of claims 12-16, wherein a phosphate buffer is used for the buffer exchange.
- 18. The method according to any one of the preceding claims, wherein imidazole, histidine or a high salt concentration15 buffer is added to the diafiltrated and buffer exchanged sample.
 - 19. The method according to claim 18, wherein imidazole is added to reach a concentration of between about 0.05 to about 20 mM.
- 20 20. The method according to any one of the preceding claims, wherein a detergent selected from a Polyoxyethylene sorbitan fatty acid ester such as Tween 20, Tween 40, Tween 60, Tween 80, and Tween 85, an alkylaryl polyether alcohol such as Triton X100, a non-ionic detergent, and a carbohydrate based
- 25 detergent such as octylglycoside, is added to the diafiltrated and buffer exchanged sample to reach a concentration of between about 0.05% (v/v) and 10% (v/v), such as about 0.1% (v/v).

39

- 21. The method according to any one of the preceding claims, wherein the IMAC step involves charging of a chromatographic medium with a divalent metal ion prior to application of the buffer exchanged sample.
- 5 22. The method according to claim 21, wherein the divalent metal ion is selected from the group consisting of Ni^{2+} , Cu^{2+} , Zn^{2+} , Co^{2+} , and Fe^{2+} , preferably Zn^{2+} .
 - 23. The method according to claim 21 or 22, wherein elution of the chromatographic medium is performed by applying
- 10 imidazole, histidine, a high salt concentration buffer, or a change of pH onto the chromatographic medium.
 - 24. The method according to claim 23, wherein elution of the chromatographic medium is performed by applying imidazole in one single step at a concentration between about 50 mM and
- 15 about 500 mM, preferably at a concentration of about 200 mM, or wherein elution is performed by applying histidine in one single step at a concentration between about 20 mM and 400 mM, preferably about 100 mM.
- 25. The method according to any one of the preceding claims,20 wherein the SEC step involves elution with a phosphate or TRIS buffer or a biological buffer, such as HEPES.
 - 26. The method according to claim 25, wherein the pH is maintained at about 7-8, preferably about 7.5.
- 27. The method according to claim 25 or 26, wherein the
 25 average pore size of the SEC matrix separates globular protein between 10 kDa and 600 kDa.
 - 28. The method according to any of the preceding claims, wherein samples containing the EGFR family derived protein

40

obtained from SEC, if necessary, is diluted before the AIE step so as to adjust the phosphate concentration to less than 15 mM, such as to the range between 10 and 12.5 mM.

- 29. The method according to any one of the preceding claims, 5 wherein the AIE step involves loading of the sample containing the EGFR family derived protein obtained after SEC on a strong or weak anion exchange matrix.
- 30. The method according to claim 29, wherein elution is performed with a buffered NaCl solution at a pH between 7 and 10 8.
 - 31. An immunogenic variant of HER-2 protein that comprises the amino acid sequence set forth in SEQ ID NO: 2, residues 17-677.
- 32. The immunogenic variant of HER-2 protein according to 15 claim 31 that consists of the amino acid sequence set forth in SEQ ID NO: 2, residues 1-677.
 - 33. A nucleic acid fragment that encodes the immunogenic variant of HER-2 protein according to claim 31 or 32.
- 34. The nucleic acid fragment according to claim 33, which is 20 a DNA fragment.
 - 35. A vector carrying the nucleic acid fragment according to claim 33 or 34.
 - 36. The vector according to claim 34, which is capable of autonomous replication.

41

- 37. The vector according to claim 34 or 36 being selected from the group consisting of a plasmid, a phage, a cosmid, a mini-chromosome, and a virus.
- 38. The vector according to any one of claims 34-37, which is 5 an expression vector.
- 39. The vector according to claim 38, comprising in the 5'→3' direction and in operable linkage, a promoter for driving expression of the nucleic acid fragment according to claim 33 or 34, optionally a nucleic acid sequence encoding a leader
 10 peptide enabling secretion of or integration into the membrane of the polypeptide fragment, the nucleic acid fragment according to claim 33 or 34, and optionally a nucleic acid sequence encoding a terminator
- 40. A transformed host cell carrying the vector of any one of 15 claims 34-39.
- 41. A stable cell line which carries the vector according to claim 38 or 39 and which expresses the nucleic acid fragment according to claim 33 or 34, and which optionally secretes or carries the immunogenic variant of HER-2 protein according to claim 31 or 32 on its surface.
- 42. An immunogenic composition for immunizing against HER-2 protein in a human comprising the immunogenic variant of HER-2 protein according to claim 31 or 32 in admixture with a pharmaceutically acceptable carrier or vehicle and optionally 25 an adjuvant.
 - 43. An immunogenic composition for immunizing against HER-2 protein in a human comprising the vector according to claim 38

15450DX00

42

- or 39 in admixture with a pharmaceutically acceptable carrier or vehicle and optionally an adjuvant
- 44. A method for immunizing a human against autologous HER-2, the method comprising administering an immunogenically
- 5 effective amount of
 - the immunogenic variant of HER-2 protein according to claim 31 or 32, or
 - the immunogenic composition according to claim 42, or
 - the vector according to claim 38 or 39, or
- 10 the immunogenic composition according to claim 43, to the human being.
 - 45. The method according to claim 44 wherein the immunization against autologous HER-2 protein is used for treating or ameliorating cancer.

Modtaget PVS 25 JUN; 2003

1

SEQUENCE LISTING

```
<110> Pharmexa A/S
<120> PURIFICATION OF HER-2 VARIANTS
<130> P1020DK00
<160> 2
<170> PatentIn version 3.2
<210>
       1
       5661
<211>
<212>
      DNA
<213> Artificial sequence
<220>
<223> Recombinant expression plasmid derived from pMT
<220>
<221> polyA_signal
<222>
       (263)...(268)
<223> SV40 late polyadenylation site
<220>
<221> misc_feature
<222>
      (157\overline{9})..(2439)
<223> Ampicillin resistance gene, encoded by complementary strand
<220>
<221> promoter
<222>
       (3050)..(3415)
<223> Metallothionein promoter
<220>
<221> RBS
<222>
       (3493)..(3501)
<223> Kozak-like sequence
<220>
<221> CDS
<222>
       (3502)..(5592)
<223> DNA encoding immunogenic, his-tagged variant of human HER-2
<220>
<221> sig_peptide
<222> (3502)..(3555)
<223> BiP signal sequence
<220>
<221> misc_feature
<222>
       (355\overline{6})..(3597)
<223> Histidine tag
<220>
<221>
       mat_peptide
<222>
       (3556) . . (5589)
```

2

<220> <221> misc_feature <222> (3598)(3603) <223> Dipeptidase stop sequence	
<220> <221> misc_feature <222> (3604)(5589) <223> Gene coding for the hHER2MA5-5DUR protein	
<220> <221> misc_feature <222> (4357)(4401) <223> Diphtheria toxoid P2 epitope	
<pre><220> <221> misc_feature <222> (5500)(5562) <223> Diphtheria toxoid P30 epitope</pre>	
<400> 1 ggccgctcga gtctagaggg cccttcgaag gtaagcctat ccctaaccct ctcctcggtc 6	50
togattetac gcgtaccggt catcaccac atcaccattg agtttaaacc cgctgatcag 12	20
cetegactyt geettetaag atceagacat gataagatae attgatgagt ttggacaaac 18	30
cacaactaga atgcagtgaa aaaaatgctt tatttgtgaa atttgtgatg ctattgcttt 24	10
	00
gtttcaggtt cagggggagg tgtgggaygt tttttaaagc aagtaaaacc tctacaaatg 36	50
toolet and matter and	20
atagetgttt cetgtgtgaa attgttatee geteacaatt ceacacaaca taegageegg 48	30
aagcataaag tgtaaagcet ggggtgeeta atgagtgage taaeteacat taattgegtt 54	10
gegeteantg eccgetttee agtegggaaa cetgtegtge eagetgeatt aatgaategg 60	00
ccaacycycg gggagaggcq gtttgcgtat tgggcgctct tecgetteet egeteaetga 66	60
ctcgctgcgc toggtcgttc ggctgcggcg ageggtatca gctcactcaa aggcggtaat 72	20
acggttatcc acagaatcag gggataacgc aggaaagaac atgtgagcaa aaggccagca 78	80
anaggccagg aaccgtaaaa aggccgcytt yctggcgttt ttccataggc tccgccccc 84	40
Annana and and	00
Anna and an anna an anna an anna an anna an anna an an	60
gettacegga tacetgteeg cettteteee ttegggaage gtggegettt eteatagete 102	20
acgctgtagg tateteagtt eggtgtaggt egttegetee aagetggget gtgtgeaega 108	80
accoccegtt cageocgace getgegeett atceggtage tategtettg agtecaacce 114	40
ggtaagacac gacttatege caetggeage agecactggt aacaggatta geagagegag 120	00

3

gtatgtagge ggtgctacag agttettgaa gtggtggeet aactaegget acactagaag 1260 1320 gacagtattt ggtatctgcg ctctgctgaa gccagttacc ttcggaaaaa gagttggtag ctcttgatcc ggcaaacaaa ccaccgctgg tagcggtggt ttttttgttt gcaagcagca 1380 gattacgcgc agaaaaaaag gatctcaaga agatcetttg atetttteta eggggtetga 1440 1500 cyctcagtyg aacgaaaact cacyttaagy gattttgytc atgagattat caaaaaggat cttcacctag atccttttaa attaaaaatg aagttttaaa tcaatctaaa gtatalalga 1560 gtaaacttgg totgacagtt accaatgett aatcagtgag gcacctatot cagegatotg 1620 1680 totatttogt toatocatag ttgcctgact coccqtcgtg tagataacta cgatacggga 1740 gggcttacca tetggcccca gtgctgcaat gataccgcga gacccacgct caccggctcc agatttatca gcaataaacc agccagccgg aagggccgag cgcagaagtg gtcctgcaac 1800 1860 tttatccgcc tecatecagt ctattaattg ttgccgggaa gctagagtaa gtagttcgcc agttaatagt ttgcgcaacq ttgttgccat tgctacaqqc atcgtgqtqt cacqctcgtc 1920 gtttggtatg yelleattea geteeggtte ceaaegatea aggegagtta catgateece 1980 catgttgtgc aaaaaagcgg ttagctcctt cggtcctccg atcgttgtca gaagtaagtt 2040 ggccgcagtg ttatcaotca tggttatggc agcactgcat aattctctta ctgtcatgcc 2100 atccgtaaga tgcttttctg tgactggtga gtactcaacc aagtcattct gagaatagtg 2160 2220 tatgeggega cegagttgot ettgecegge gteaatacgg gataataceg egceacatag 2280 cagaacttta aaagtgctca tcattggaaa acgttcttcg gggcgaaaac tctcaaggat ettaccgotg ttgagatcca gttcgatgta acccactcgt gcacccaact gatcttcagc 2340 atcttttact ttcaccageg tttctgggtg agcaaaaaca ggaaggcaaa atgccgcaaa 2400 aaagggaata agggegacac ggaaatgttg aatactcata ctcttccttt ttcaatatta 2460 ttgaagcatt tatcagggtt attgtctcat gagcggatac atatttgaat gtatttagaa 2520 2580 aaataaacaa ataggggtto ogogcacatt toccogaaaa gtgccacctg acgtotaaga 2640 ascettatt atcatgacat taacctataa aaataggogt atcacgaggo cotttogtto gcgcgtttcg gtgatgacgg tgaaaacctc tgacacatgc agctcccgga gacggtcaca 2700 2760 gettgtetgt aageggatge egggageaga caagecegte agggegegte agegggtgtt ggcgggtgto ggggctggct taactatgcg gcatcagagc agattgtacl yayaytgcac 2820 catatgcggt gtgaaatacc gcacagatgc gtaaggagaa aataccgcat caggcgccat 2880 2940 tegecatica ggetgegeaa etgttgggaa gggegategg tgegggeete ttegetatta 3000 cgccagctgg cgaaaggggg atgtgctgca aggcgattaa gttgggtaac gccagggttt

4

tcccagtc	ac gacg	ttgtaa aa	cgacggcc	agtgc	cagtg a	attaattc	g ttgca	ggaca	3060
ggatgtgg	tg cccg	atgtga ct	agctctt	gctgc	aggcc ç	gtectatec	t ctggt	tccga	3120
taagagac	cc agaa	ctccgg c	ccccacco	cecae	ecgcca (ccccatac	a tatgt	ggtac	3180
gcaagtaa	ga gtgc	ctgcgc at	gececate	g tgccc	cacca e	agagttttg	c atccc	ataca	3240
agtcccca	aa gtgg	agaacc ga	aaccaatto	ttcgc	ogggca (gaacaaaag	c ttctg	cacac	3300
gtctccac	tc gaat	ttggag c	caaccaac	g tgtgd	caaaag a	aggtgaato	g aacga	aagac	3360
ccgtgtgt	aa agoc	gcgttt c	caaaatgta	a taaaa	accgag	agcatctgg	gc caato	tgcat	3420
cagttgtg	gt cago	agcaaa a	tcaagtgaa	a tcato	ctcagt	gcaactaaa	ag ggggg	gateta	3480
gategggg	jta ccaa	agtcac c		Leu C		ttg ctg (Leu Leu)			3531
						caa cac (Gln His (5			3579
						gtg tgt Val Cys 20			3627
						acc cac Thr His			3675
				Gln V		cag gga Gln Gly			3723
						ttc ctg Phe Leu			3771
						aac caa Asn Gln 85			3819
						acc cag Thr Gln 100			3867
			a Val Lev			Asp Pro			3915
				r Pro (ctg cgg Leu Arg		Gln	3963
		u Thr Gl				gtc ttg Val Leu			4011

5

aac Asn	ccc Pro	cag Gln 155	ctc Leu	tgc Cys	tac Tyr	cag Gln	gac Asp 160	acg Thr	att Ile	ttg Leu	tgg Trp	aag Lys 165	gac Asp	atc Ile	ttc Phe	4059
					ctg Leu											4107
					tgt Cys 190											4155
					gat Asp											4203
Gly	ggc Gly	tgt Cys	gcc A1.a 220	cgc Arg	tgc Cys	aag Lys	Gly	cca Pro 225	ctg Leu	eec Pro	act Thr	gac Asp	tgc Cys 230	tgc Cys	cat His	4251
gag Glu	cag Gln	tgt Cys 235	gct Ala	gcc Ala	Gly ggc	tgc Cys	acg Thr 240	Gly	ccc Pro	aag Lys	cac His	tct Ser 245	gac Asp	tgc Cya	ctg Leu	4299
gcc Ala	tgc Cys 250	ctc Leu	cac His	ttc Phe	aaç Asn	cac His 255	agt Ser	Gly	atc Ile	tgt Cys	gag Glu 260	Leu	cac His	tgc Cys	cca Pro	4347
gcc Ala 265	ctg Leu	gtc Val	cag Gln	tac Tyr	atc Ile 270	aaa Lys	gct Ala	aac Asn	tcc Ser	aaa Lys 275	Phe	atc Ile	ggt Gly	atc Ile	acc Thr 280	4395
gag Glu	ctg Leu	cgg Arg	tat Tyr	aca Thr 285	Phe	GJ y	gcc Ala	agc Ser	tgt Cys 290	Val	act The	gcc Ala	tgt Cys	ecc Pro 295	tac Tyr	4443
aac Asn	tac Tyr	ctt Leu	tct Ser 300	Thr	gac Asp	gtg Val	gga Gly	Sox 305	Cys	acc	Leu	gtc Val	tgc Cys 310	Pro	ctg Leu	[*] 4491
cac Nis	aac Asn	Gln 315	Glu	gtg Val	aca Thr	gca Ala	gag Glu 320	Asp	gga Gly	aca Thr	Gl:	cgg Arg 325	Cys	gag Glu	aag Lys	4539
tgc Cys	agc Ser 330	Lys	ccc Pro	tgt Cys	gcc Ala	cga Arg 335	Val	tgc Cys	tat Tyr	ggt	Lev 340	ı Gly	atg Met	gag Glu	cac His	4587
ttg Len 345	Arg	gag Glu	gtg Val	agg Arg	gca Ala 350	gtt Val	acc	agt Ser	gcc Ala	aat Asn 355	Ile	cag Gln	gag Glu	ttt Phe	gct Ala 360	4635
GJ A	tgc Cys	aag Lys	aag Lys	atc Ile 365	Phe	er A aaa	ago Sez	: ctg	gca Ala 370	Phe	cto Lev	g eeg Pro	gag Glu	ago Ser 375	ttt Phe	4683
gat Asp	ggg	gac 'Asp	CCA Pro 380	Ala	tcc Ser	aac Asn	act Thr	gcc Ala 385	e Pro	cto Lev	caç	g cca	gaç Glu 390	Glr	g ctc n Leu	4731

6

caa Gln	gtg Val	ttt Phe 395	gag Glu	act Thr	ctg Leu	gaa Glu	gag Glu 400	atc Ile	aca Thr	ggt	tac Tyr	cta Leu 405	tac Tyr	atc Ile	tca Ser	4779
					ctg Leu											4827
gta Val 425	atc Ile	Arg	gga Gly	Ary Cga	att Ile 430	ctg Leu	cac His	aat Asn	ggc Gly	gcc Ala 435	tac Tyr	tcg Ser	ctg Leu	acc Thr	ctg Leu 440	4875
caa Gln	ej gag	ctg Leu	ggc Gly	atc Ile 445	agc Ser	tgg Trp	ctg Leu	G1 y ggg	ctg Leu 450	ege Arg	tca Ser	ctg Leu	agg Arg	gaa Glu 455	ctg Leu	4923
GJ'À Gàc	agt Ser	gga Gly	ctg Leu 460	gcc Ala	ctc Leu	atc Ile	cac His	cat His 465	aac Asn	acc Thr	cac His	ctc Leu	tgc Cys 470	ttc Phe	gtg Val	4971
cac His	acg Thr	gtg Val 475	CCC	tgg Trp	ysb dac	cag Gln	ctc Leu 480	ttt Phe	Arg	aac Asn	ccg Pro	cac Nis 485	caa Gln	gct Ala	ctg Leu	5019
ctc Leu	Cac His 490	act Thr	gcc Ala	aac Asn	cgg Arg	cca Pro 495	gag Glu	Asp gac	gag Glu	tgt Cys	gtg Val 500	Gly	gag Glu	G] À	ctg Leu	5067
gcc Ala 505	tgc Cys	cac His	cag Gln	ct.g Leu	tgc Cys 510	gcc Ala	cga Arg	ej A aaa	cac His	tgc Cys 515	tgg Trp	GTA Gaf	cca Pro	Gly	Pro 520	5115
aco Thr	cag Gln	tgt Cys	gto Val	aac Asn 525	Cys	agc Ser	cag Gln	ttc Phe	Ctt Leu 530	Arg	ggc Gly	cag Gln	gag Glu	tgc Cys 535	gtg Val	5163
gag Glu	gaa Glu	tgc Cys	cga Arg 540	Val	ctg Lou	cag Gln	CJ A	Leu 545	Pro	agg Arg	gay Glu	tat Tyr	gtg Val 550	Asn	gcc Ala	5211
agg Arg	cac His	tqt Cys 555	Leu	CCG Pro	tgc Cys	cac His	Pro 560	Glu	tgt Cys	cag Gln	CCC Pro	cag Gln 565	Asn	ggc	tca Ser	5259
gtg Val	acc Thr 570	Cys	ttt Phe	gga Gly	ccg Pro	gag Glu 575	Ala	gac Asp	cag Gln	tgt Cys	gtg Vai 580	. Ala	tgt Cys	gcc Ala	cac His	5307
tat Tyr 585	Lys	Asp	e cct	Pro	ttc Phe 590	Cys	gtg Val	gec Ala	cgc Arg	tgo Cys 595	Pro	agc Ser	ggt Gly	gto Val	Lys 600	5355
Pro	gac Asp	cto Lev	tcc Sex	tac Tyx 605	Met	Pro	ato Ile	tgo Trp	aag Lys 610	Phe	. cca	gat Asp	gag Glu	gaq Glu 619	g Gly g ggc	5403
gca Ala	tgc Cys	cag Gln	Pro 620	Cys	CCC Pro	ato Ile	aac Ası	tgo Cys 625	The	cac His	tco Ser	tgt Cys	gtg Val	Asp	c ctg Leu	5451

7

gat Asp	gac Asp	eag Lys 635	ggc Gly	tgc Cys	Pro	gcc Ala	gag Glu 640	cag Gln	aga Arg	gcc Ala	agc Ser	ect Pro 645	ctg Leu	acg Thr	tcc Ser	5499
ttc Phe	aac Asn 650	aac Asn	ttc Phe	acc Thr	gtg Val	agc Ser 655	ttc Phe	tgg Trp	ctg Leu	Arg	gtg Val 660	ccc Pro	aag Lys	gtg Val	agc Ser	5547
gcc Ala 665	agc Ser	cac His	ctg Leu	gag Glu	atc Ile 670	gtc Val	tct Ser	gcg Ala	gtg Val	gtt Val 675	GTA GGC	att Ile	ctg Leu			5589
taga	agct	ttg g	gtaco	gago	et cç	gato	cact	agt	ccaç	gtgt	ggt	gaat	tc t	gca	gatate	5649
cago	aca	gtg q	ic													5661
<210 <210 <210 <210	l> 2>	2 696 PRT Arti	fici	al se	equer	ıce										
<22 <22		Recor	nbina	ent e	expre	essi	on p	lasm.	id d	eriv	ed f	com j	oSI	٠		
<40)> :	2														
Met	Lys	Leu	Cys -15	Ile	Leu	Leu	Ala	Val -10	Val	Ala	Phe	Val	Gly -5	Leu	Ser	
Leu	Gly -1		Lys	His	Gln	His 5	Gln	His	Gln	Ilis	Gln 10	His	Gln	His	Gln	
Ala 15	Pro	Ser	Thr	Gln	Val 20	Суз	Thr	Gly	Thr	Asp 25	Met	ГÀЗ	Leu	Arg	Leu 30	
Pro	Ala	Ser	Pro	Glu 35	Thr	His	Ьea	Asp	Met 40	Leu	Arg	His	Leu	Тут 45	Gln	
Gly	Cys	Gln	Val 50	Val	Gln	Gly	Asn	Leu 55	Glu	Leu	Thr	Tyr	Leu 60	Pro	Thr ·	
Asn	Ala	Ser 65	Leu	Sor	Phe						Glu			Gly	Tyr	
Val	Leu 80	Ile	Ala	His	Asn	G1n 85	Val	Arg	Gln	Val	Pro 90	Leu	Gln	Arç	Leu	
Arg 95	Ile	Val	Arg	Gly	Thr 100		Leu	Phe	GLu	Asp 105		Týr	Ala	ī.ev	Al.a 110	

8

Val Leu Asp Asn Gly Asp Pro Lou Asn Asn Thr Thr Pro Val Thr Gly
115 120 125

Ala Ser Fro Gly Gly Leu Arg Glu Leu Gln Leu Arg Ser Leu Thr Glu 130 135 140

Ile Leu Lys Gly Gly Val Leu Ile Gln Arg Asn Pro Gln Leu Cys Tyr 145 150 155

Gln Asp Thr Ile Leu Trp Lys Asp Ile Phe His Lys Asn Asn Gln Leu 160 165 170

Ala Leu Thr Leu Ile Asp Thr Asn Arg Ser Arg Ala Cys His Pro Cys 175 180 185 190

Ser Pro Met Cys Lys Gly Ser Arg Cys Trp Gly Glu Ser Ser Glu Asp 195 200 205

Cys Gln Ser Leu Thr Arg Thr Val Cys Ala Gly Gly Cys Ala Arg Cys 210 215 220

Lys Gly Pro Leu Pro Thr Asp Cys Cys His Glu Gln Cys Ala Ala Gly 225 230 235

Cys Thr Gly Pro Lys His Ser Asp Cys Leu Ala Cys Leu His Phe Asn 240 245 250

His Ser Gly Ile Cys Glu Leu His Cys Pro Ala Leu Val Gln Tyr Ile 255 260 265 270

Lys Ala Asn Ser Lys Phe Ile Gly Ile Thr Glu Leu Arg Tyr Thr Phe 275 280 285

Gly Ala Ser Cys Val Thr Ala Cys Pro Tyr Asn Tyr Leu Ser Thr Asp 290 295 300

Val Gly Ser Cys Thr Leu Val Cys Pro Leu His Asn Gln Glu Val Thr 305 310 315

Ala Glu Asp Gly Thr Gln Arg Cys Glu Lys Cys Ser Lys Pro Cys Ala 320 325 330

Arg Val Cys Tyr Gly Leu Gly Met Glu His Leu Arg Glu Val Arg Ala 335 340 345 350

15450DX00

9

Val Thr Ser Ala Asn Ile Gln Glu Phe Ala Gly Cys Lys Ile Phe 355 360 365

Gly Ser Lou Ala Phe Leu Pro Glu Ser Phe Asp Gly Asp Pro Ala Ser 370 375 380

Asn Thr Ala Pro Leu Gln Pro Glu Gln Leu Gln Val Phe Glu Thr Leu 385 390 395

Glu Glu Ile Thr Gly Tyr Leu Tyr Ile Ser Ala Trp Pro Asp Ser Leu 400 405 410

Pro Asp Leu Ser Val Phe Gln Asn Leu Gln Val Ile Arg Gly Arg Ile 415 420 425 430

Leu His Asn Gly Ala Tyr Ser Leu Thr Leu Gln Gly Leu Gly Ile Ser 435 440 445

Trp Leu Gly Leu Arg Ser Leu Arg Glu Leu Gly Ser Gly Leu Ala Leu 450 455 460

Ile His His Asn Thr His Leu Cys Phe Val His Thr Val Pro Trp Asp
465 470 475

Gln Leu Phe Arg Asn Pro His Gln Ala Leu Leu His Thr Ala Asn Arg 480 485 490

Pro Glu Asp Glu Cyo Val Gly Glu Gly Leu Ala Cys His Gln Leu Cys 495 500 505 510

Ala Arg Gly His Cys Trp Gly Pro Gly Pro Thr Gln Cys Val Asn Cys 515 520 525

Ser Gln Phe Leu Arg Gly Gln Glu Cys Val Glu Glu Cys Arg Val Leu 530 535 540

Gln Gly Leu Pro Arg Glu Tyr Val Asn Ala Arg His Cys Leu Pro Cys 545 550 555

His Pro Glu Cys Gln Pro Gln Asn Gly Ser Val Thr Cys Phe Gly Pro 560 570

Glu Ala Asp Gln Cys Val Ala Cys Ala His Tyr Lys Asp Pro Pro Phe 575 580 585

10

Cys Val Ala Arg Cys Pro Ser Gly Val Lys Pro Asp Leu Ser Tyr Met 595 600 605

Pro Ile Trp Lys Phe Pro Asp Glu Glu Gly Ala Cys Gln Pro Cys Pro 610 620

Ile Asn Cys Thr His Ser Cys Val Asp Leu Asp Asp Lys Gly Cys Pro 625 630 635

Ala Glu Gln Arg Ala Ser Pro Leu Thr Ser Phe Asn Asn Phe Thr Val

Ser Phe Trp Leu Arg Val Pro Lys Val Scr Ala Ser His Leu Glu Ile 655 660 665 670

Val Ser Ala Val Val Gly Ile Leu 675

Modtaget PVS 25 JUN: 2003

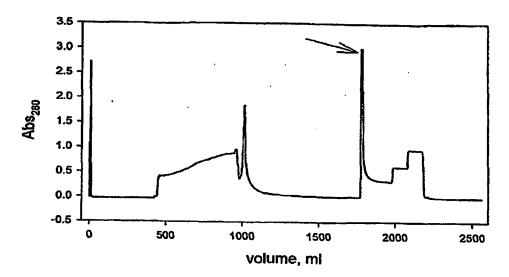


Fig. 1

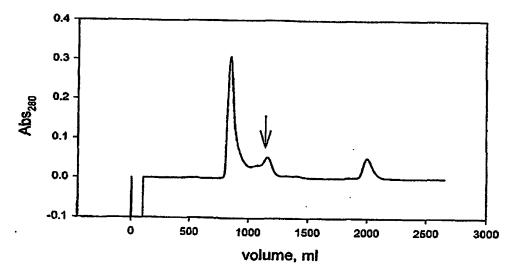


Fig. 2

25 JUN, 2363

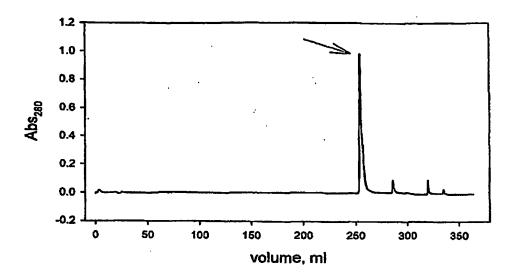


Fig. 3

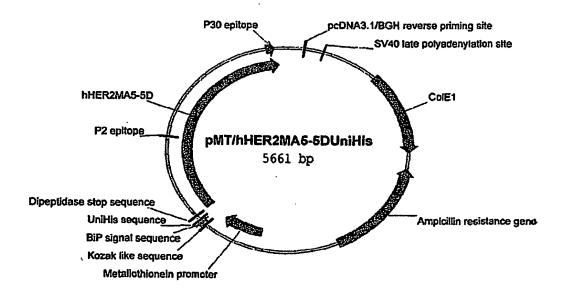


Fig. 4

This Page is Inserted by IFW Indexing and Scanning Operations and is not part of the Official Record

BEST AVAILABLE IMAGES

Defective images within this document are accurate representations of the original documents submitted by the applicant.

Defects in the images include but are not limited to the items checked:

BLACK BORDERS
☐ IMAGE CUT OFF AT TOP, BOTTOM OR SIDES
☐ FADED TEXT OR DRAWING
☐ BLURRED OR ILLEGIBLE TEXT OR DRAWING
☐ SKEWED/SLANTED IMAGES
☐ COLOR OR BLACK AND WHITE PHOTOGRAPHS
GRAY SCALE DOCUMENTS
LINES OR MARKS ON ORIGINAL DOCUMENT
☐ REFERENCE(S) OR EXHIBIT(S) SUBMITTED ARE POOR QUALITY
OTHER:

IMAGES ARE BEST AVAILABLE COPY.

As rescanning these documents will not correct the image problems checked, please do not report these problems to the IFW Image Problem Mailbox.